# **Generation of Transportation Fuel from Solid Municipal Waste Plastics**

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#### ABSTRACT

Waste plasti cs are one of t he biggest environmental co ncerns t he w orld face s t oday. The am ount of waste pl astics i s i ncreasing rapidly each day. Waste plastics exposure to the environment is very hazardous. Over tim e waste plastics p hoto-degrade a nd bec ome ver y t iny dust particles. These dust particles contain very harmful com pounds i ncluding benzene, s ulfur, carbon and many ot hers. A ccording to studies, waste plastic's components are one of the biggest reasons for the depletion of the ozone layer and contributor of g lobal warm ing. Man y scien tists have been tryin g to fi gure out to utilize these waste plastics and convert them into useful energy source. It is po ssible to convert waste plastics into energy because they are made from petroleum. They have s ucceeded in de veloping many m ethods in cluding pyrolysis, catalytic cracking, thermal degrading and others. Natural State Researc h Inc. (NSR ) has been working with t he t hermal degra dation process a nd was successful in extracting fuel from waste pl astics at 370 – 420 degree C.

*Keywords:* Waste plastics, Fuel, FT-IR, Degradation, Hydrocarbon, G C/MS, Ther mal, Cracking

#### **INTRODUCTION**

Plastic are m acromolecules, formed by polymerization of hy drocarbon materials and i t has the ability to be shaped by the application of reasonable amount of heat a nd press ure making them very easy to use i n our daily lives. These plastics are made from crude oil a limited energy source. Plastic are being used all over the world for all sorts of activ ities and afterward s th ese plastics are becom ing wa ste plastics. Waste plastics do not biodegrade in landfills and are not easily recycled and degrade in quality during the recycling process causing people to dump them in land fill. This m ethod of dumping requires a lot effort and money.

Not only on land but waste plastics are causing problems in the sea region as well. Research conducted by Charles J. M oore (Long Beach California) a bout the Great Pacific Garbage Patc h s hows t he horror and impacts waste plastic can have on oceanic and marine life. According to his s tudy th e G arbage P atch is estimated to be twice t he size of Te xas and contains ~3.5 million tons of waste material and 80% of it is waste plastic litter [1].

Methods have been developed to u tilize these waste plastics and conver t them in to low cost and environmentally friendly fuels. If carried out properly t his m ethod ca n help sa ve t he environment and the economy. Some methods of conversion of waste plastics into fuel include pyrolysis [2-3], thermal degradation [4-6], catalytic cracking [7-8] and others. The current commercial fuel is a hazard to the environment. Emissions fr om evaporated fuel includes unburned hy drocarbons, w hich are responsible for gr ound-level ozo ne and smog; ni trogen oxides ( $NO_x$ ), w hich c ontribute t o oz one an d acid rain; ca rbon m onoxide (CO), a toxic byproduct of in complete combustion and a health h azard; su lfur dioxide (SO<sub>2</sub>), w hich contributes t o aci d rai n; a nd car bon dioxide  $(CO_2)$ , a gre enhouse gas t hat contributes to global warming.

These fuels derived form wastes plastic s are expected to be m uch more environm entally friendly than the conventional fuels and since the raw res ource of waste plas tics are seem ingly unlimited, th e production of the fuel will be relatively less.

Natural State Research Inc. (NSR) has developed such m ethod where the waste plastics are

collected fr om various su permarkets and o ther places and convert them into liquid hydrocarbon fuels.

## **PROCESS DESCRIPTION**



Figure 1: NSR fuel production process

NSR discovered a process that uses therm al degradation to heat t he waste plastic to form liquid slurry; at a t emperature ranging from 370 -420 <sup>0</sup> C with catalyst, then the liquid slurry turns into v apor, that v apor is then condensed (see figure 1) to produce the liquid hydrocarbon fuels titled NSR Fuel. It should be noted that no chemicals are used to carry out this process and the end product is filtered u sing a commercial fuel purifier that operat e using coalescence and centrifugal force. Duri ng t he pr ocess som e valuable ligh t g as is produ ced. Th at gas is cleaned using a gas scrubber and collected using a pump and storage gas cylinder. This light gas can be used to heat the plastics to produce fuel saving cost for fuel production.

Experiments in a lab scale have been performed with m ajority of t he waste p lastic typ es: h igh density pol vethylene (HDPE, co de 2), 1 ow density p olvethylene (LDPE, c ode 4), polypropylene (PP, code 5), and polystyrene (PS, code 6). These plastic types were investigated singly and in combination with each other. In a laboratory scale, the weight of a single batch of input p lastic for the fuel p roduction process ranges fr om 2 50 gr ams to 4 k ilograms. The waste plastics are c ollected, optionally sorte d, cleaned of contamination or without clean ing and grinded into small pieces prior to the thermal liquefaction p rocess. The produced f uel has density of 0.77 g/ml. W ith 1 ki logram (kg) of waste plastic about 1200 - 1300 ml of NSR fuel can be p roduced. Also p roducing 1 gallon of fuel requires 12-13 kWh which is about \$1.32 in laboratory scale. When fully commercialized the production amount will increase and the cost will decrease hal f. The end products consist of 90% of liquid hydrocarbon fuel 5% light gas (C1-C4) (Methane, Ethane, Propane and Butane) and 5% solid residue.

Sample Name	Inflection Point in	On Set Temperatu
	Temperature	re
	(° C)	(° C)
LDPE 4	466.16	436.23
HDPE 2	477.96	450.40
PS 6	364.88	326.62
PP 5	403.72	359.63

**Table 2:** T hermo-gravimetric A nalysis (TGA)Results of Waste Plastic Samples

Plastic Name	Density g/cm <sup>3</sup>	
LDPE 4	0.92-0.94	
HDPE 2	0.95-0.97	
PP 5	0.90-0.91	
PS 6	1.05-1.07	

**Table 3:** Physical properties of virgin plastics

Plastic Name	Melting Point	
	(° C)	
LDPE 4	120	
HDPE 2	130	
PP 5	160	
PS 6	240	

**Table 4**: Melting points of virgin plastics

#### **FUEL ANALYSIS**



Figure 5: Gas Chromatogram of NSR Fuel

The NSR fuel carbon c hain ranges from (C3-C27). These data indicates that the NSR fuels have a wi de range of hydrocarbon g roups resulting in a h igher th ermal content. The thermal content allows the fuel to burn for longer period of time resulting in efficiency when used in compatible engines.



**Figure 6:** Differential Scan ning Calorimeter (DSC) graph of NSR Fu el indicating the boiling point

The DSC graph indicates the peak boiling point a substance c an reach. In this case the NSR fuel has a p eak b oiling point of  $149.26^{-0}$  C and a Delta H value of 12247.7270 j/g. that indicates the enthalpy value of the fuel.



Figure 7: FT-IR spectra of NSR Fuel

The compounds present in the NSR fuel are as follows: H Bonded NH, CH2 , C- CH3,Non Conjugated, Non C onjugated, Am ides, C  $H_2$ , Acetates, -C H= CH  $_2$ , -CH=CH-, C=  $CH_2$ , - CH=CH- (cis).



Figure 8: FT-IR library search compound list

Elemental Analyzer (E A-2400) result under CHNS m ode indicates that NSR fuel contains 85.61 % car bon, 13.10% Hy drogen, 0.3 % Nitrogen and 2.26% Sulfur.

Sample	Test	Result
Property	Method	
Gross Heat	ASTM-D240 12	7,413
of		BTU/gal
Combustion		_
(BTU)		
API Gravity	ASTM-D4052	
Barometric	ASTM-D86	760 mm Hg
pressure		
IBP recovery	ASTM-D86	109.5 °F
10%	ASTM-D86 24	6.2 °F
recovery		
50%	ASTM-D86 48	7.0 °F
recovery		
FBP	ASTM-D86 63	3.5 °F
recovery		
Residue ASTN	1 -D86	28.2 Vol%
Corrected	ASTM-D86 1.	2 Vol%
loss		
Corrected	ASTM-D86 70	.6 Vol%
Recovery		
Pour Point	ASTM-D97	9 °C
Cloud Point	ASTM-D2500	12 °C
Freezing	ASTM-D2386 1	2.0 °C
Point		
Conductivity A	STM-D2624	2 pS/M
Sulfur	ASTM-D5453 2	.8 mg/kg
Content		
ASTM Color	ASTM-D1500	1.5
Water	ASTM-E203 37	mg/kg
Content –		
Karl Fischer		
Vanadium	ASTM-D5708 <	1 .00 mg/kg
content		
Nickel	ASTM-D5708 <	1 .00 mg/kg
content		
Iron content	ASTM-5708	2.70 mg/kg
Ash C ontent	ASTM-D482	0.001 Wt %

@ 775 °C		
Flash Poi nt-	ASTM-D93	< room temp
PMCC		°F
(procedure		
A)		
Carbon	ASTM-D4530	< 0.10 Wt %
Residue		
(MCRT)		
Acid	ASTM-D664 0.	10 mg
Number of		KOH/g
Petroleum		
Products		

**Table 9:** INTERTEK third party re port ofanalysis of the NSR Fuel

### CONCLUSION

The final NSR product is tested and proven to be compatible with all typ es' i nternal co mbustion engines. Also when used with suitable generators it can produce electricity to powe r all sorts of appliances. The NSR fuel is to be tested under all the ASTM standard test and further modification are subjected to be conducted in the future.

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## REFERENCE

[1]. C.J. Moore, S.L. M oore, M.K. Leec aster and S.B. Weisberg, "A comparison of plastic and plankton in the North Pacific Central Gy re", Al galita Marin e Research Foundation and Southern California C oastal Water Research Project; *Marine* Pollution Bulletin 42 (2001)-1297-1300.

[2]. Naresh Shah, Jeff R ockwell, and Gerald P. Huffman\*. Conversion of Waste Plastic to Oil: Direct Liqu efaction v ersus Pyrolysis and Hydroprocessing. CFFLS, 533 S. Limestone St., University of Ke ntucky, L exington, Ke ntucky 40506-0043, November 4, 1998; 832-838.

[3]. R oberto Aguado, Mart in Olazar \*, Beatriz Gaisan, Ruben Prieto, Javier Bilbao. Kinetics of polystyrene py rolysis i n a c onical s pouted bed reactor. De partmento de i ngeniera Quimica, Universidad del Pais Vasco, Apartado 644,48080 Bilbao, Spain May 2002

[4]. W. Kaminsky, B. Sc hlesselmann & C.M. Simon. T hermal de gradation o f m ixed pl astic waste to aromatics an d gas. University o f Hamburg, Institute for r Techn ical and Macromolecular Chemistry, BudesstraBe 45, D-20146 Hamburg, Germany, 2 January; 189-197.

**[5].** Ta kehiko M oriya, Hei ji E nomoto. Characteristics of polyethylene crac king in supercritical water compared to thermal cracking. 980-8759 March 1999.

**[6].** N. Miskolczi \*, L. Bartha, G. Deak, B. Jover. Thermal Degradation of municipal plastic waste for p roduction o f fuel-like hydrocarbons. Department of Hydrocarbon and Coal Processing, University os Vesz prem, Egy etem St . 10, Veszprem, H -8200, Hungary MO L Hungarian Oil and Gas PLC . R&D, PO B. 1, Szazhalombatta, H-2443, Hungary 14 April 2004

[7]. Y. Uemichi, Devel opment of a ca talytic cracking process for converting waste plastics to petrochemicals, *J. Mat. Cycles Waste Manage*, 5(2), 89-93, 2003.

**[8].** Ju ya N ishino\*, Masaak i I toh, Hironbu Fijiyoshi, Yo shi Uem ichi. Catalytic d egradation of plastic was te i nto pet rochemicals usi ng Ga - ZSM-5. C hemical engi neering department, product de velopment ce ner, I HI Coporation, 1-shin-nakahara, iso go-ku, y okohoma 2 35-8501, Japan

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