

# Direct Hydrothermal Synthesis of $\text{LiMn}_2\text{O}_4$ Spinel and Lithium Ion Selective Adsorption

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## ABSTRACT

Spinel-type ternary  $\text{LiMn}_2\text{O}_4$  oxides precursor was synthesized via directly hydrothermal synthesis of  $\text{Mn}(\text{NO}_3)_2$ ,  $\text{LiOH}$  and  $\text{H}_2\text{O}_2$  at 383 K for 8 h. The final low-dimensional  $\text{MnO}_2$  nanorod ion-sieve with lithium ion selective adsorption property was prepared further by the acid treatment process to completely extract lithium ions from the Li-Mn-O lattice. The effects of hydrothermal reaction condition on the nanostructure, chemical stability and ion-exchange property of the  $\text{LiMn}_2\text{O}_4$  precursor and  $\text{MnO}_2$  ion-sieve were systematically examined via powder X-ray diffraction (XRD), high-resolution transmission electron microscopy (HRTEM), selected-area electron diffraction (SAED),  $\text{N}_2$  adsorption-desorption and lithium ion selective adsorption measurements. The results show that this new kind of low-dimensional  $\text{MnO}_2$  nanorod could be applied in lithium extraction from aqueous environment including brine, sea-water and waste water.

**Keywords:**  $\text{LiMn}_2\text{O}_4$ , hydrothermal synthesis, low-dimensional, ion-sieve, adsorption

## 1 INTRODUCTION

$\text{LiMn}_2\text{O}_4$  is a cubic spinel with space group symmetry  $\text{Fd}3\text{m}$ . The  $\text{Li}^+$  is transported via 8a-16d-8a channels in the three-dimensional interstitial space provided by the  $[\text{Mn}_2\text{O}_4]$  framework in the  $\text{LiMn}_2\text{O}_4$  spinel with little shrinking or swelling of the spinel structure [1]. The property makes the material applicable as cathode of lithium batteries [2, 3] and selective ion-sieves for lithium adsorption from aqueous solution including brine or seawater [4, 5].

Kenta Ooi and colleagues systematically researched the  $\text{Li}^+$  selective adsorption on the  $\lambda$ - $\text{MnO}_2$  ion-sieve [6-8]. It should be noticed that the  $\text{MnO}_2$  ion-sieve obtained by conversional solid-phase reaction is of irregular morphology and large aggregate with broad particle size distribution, though improved via the optimization of the synthesis conditions [9, 10]. Rationally, the soft chemistry hydrothermal-reaction is proposed to obtain  $\text{LiMn}_2\text{O}_4$  spinel with homogeneous composition and nanosize distribution. Kenta Ooi and colleagues [11] make  $\text{LiMn}_2\text{O}_4$  spinel via the hydrothermal-reaction of  $\gamma$ - $\text{MnO}_2$  or layered compound of Li-birnessite for about 24 days or longer, yet the raw material of  $\gamma$ - $\text{MnO}_2$  or Li-birnessite has to be firstly prepared via a complicated process [12-14]. In the present

work, a much milder hydrothermal condition is optimized to synthesize low-dimensional spinel  $\text{LiMn}_2\text{O}_4$  precursor directly. The final low-dimensional  $\text{MnO}_2$  nanorod ion-sieve with lithium ion selective adsorption property was prepared further by the acid treatment process to completely extract lithium ions from the Li-Mn-O lattice; the structure characteristics and ion-exchange properties of the samples are studied by XRD, HRTEM, SAED,  $\text{N}_2$  adsorption-desorption, and lithium ion selective adsorption measurement.

## 2 EXPERIMENTAL

### 2.1 Synthesis of Low-Dimensional $\text{LiMn}_2\text{O}_4$ Precursor and $\text{MnO}_2$ Ion-Sieve

All chemicals used are AR reagents. 300 ml mixed solution of  $\text{H}_2\text{O}_2$  ( $0.20$ - $0.90 \text{ mol}\cdot\text{l}^{-1}$ ) and  $\text{LiOH}$  ( $0.70$ - $1.50 \text{ mol}\cdot\text{l}^{-1}$ ) is added dropwise into a teflon-coated stainless autoclave (1000 ml) filled with 300 ml  $0.40 \text{ mol}\cdot\text{l}^{-1}$   $\text{Mn}(\text{NO}_3)_2$  solution stirred vigorously at  $150 \text{ r}\cdot\text{min}^{-1}$ . After the mixed solution maintained in air at room temperature for 2 h, the autoclave is sealed and heated at  $343$ - $453 \text{ K}$  for  $8$ - $48 \text{ h}$  respectively, then cooled naturally to room temperature. The obtained black precipitate is filtrated, washed completely with deionized water till the conductance of filtrate reaches the same level of the deionized water (about  $18.2 \text{ M}\Omega\cdot\text{cm}^{-1}$ ) and dried at  $343 \text{ K}$  for 12 h. By optimizing the hydrothermal conditions of reaction temperature, contact time, concentration of  $\text{H}_2\text{O}_2$  and  $\text{LiOH}$  solution, pure cubic  $\text{LiMn}_2\text{O}_4$  ternary oxide, named LMO could be produced at  $383 \text{ K}$  for 8 h the mixed solution of  $0.15 \text{ mol}\cdot\text{l}^{-1}$   $\text{H}_2\text{O}_2$ ,  $0.50 \text{ mol}\cdot\text{l}^{-1}$   $\text{LiOH}$  and  $0.20 \text{ mol}\cdot\text{l}^{-1}$   $\text{Mn}(\text{NO}_3)_2$ . The  $\text{Li}^+$  extraction from  $\text{LiMn}_2\text{O}_4$  precursor is carried out in  $0.10 \text{ mol}\cdot\text{l}^{-1}$   $\text{HCl}$  solution at  $303 \text{ K}$  until the lattice  $\text{Li}^+$  is completely extracted (*in situ* measured by Metrohm 861 Advanced Compact Ion Chromatograph). The acid-treated materials are filtered, washed with deionized water and dried at  $333 \text{ K}$  for 8 h to obtain the final  $\text{MnO}_2$  ion-sieve, named SMO. The whole process involves hydrothermal precipitation and redox procedure as the reaction (1) including three steps as equations (2)-(4). At high  $\text{LiOH}$  concentration ( $1.00 \text{ mol}\cdot\text{l}^{-1}$ ) the  $\text{Mn}^{\text{II}}(\text{OH})_2$  is oxidized accompanied with the  $\text{Li}^+$  insertion into the Mn-O lattice to form the  $\text{LiMn}^{\text{III}}\text{Mn}^{\text{IV}}\text{O}_4$  tri-oxide precursor.

Total reaction:



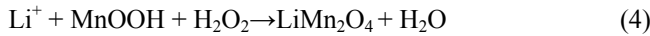
Precipitation reaction:



Redox reaction:



$\text{Li}^+$  insertion:



## 2.2 Characterization of Samples

The bulky phase purity of the material is examined via X-ray diffraction (XRD) analysis using a Rigaku D/max 2550 X-ray diffractometer with Cu  $K_\alpha$  radiation ( $\lambda=1.54056 \text{ \AA}$ ), operating at 40 kV, 100 mA and scanning rate of  $10^\circ \cdot \text{min}^{-1}$ . The microstructure and surface morphology of the samples are analyzed by HRTEM and SAED on a JEOL JEM-2100F TEM (200 kV) after the samples are dispersed by ultrasonic in anhydrous ethanol for 5 min and then placed onto the cuprum grid for observations. The texture detail is characterized by  $\text{N}_2$  adsorption-desorption at 77 K using Micromeritics ASAP 2010 V5.02, and the surface area is calculated from the Brunauer-Emmett-Teller (BET) equation, and pore volume from the total amount of nitrogen adsorbed at relative pressures of ca. 0.96 with Barrett-Joyner-Halenda (BJH) equation.

## 2.3 Lithium Ion Adsorption Measurement

The  $\text{Li}^+$  adsorption isotherm is carried out by stirring ( $150 \text{ r} \cdot \text{min}^{-1}$ ) about 100 mg ion-sieve in 100 ml LiCl solution (pH = 10.1 adjusted by buffer solution comprised of  $0.1 \text{ mol} \cdot \text{l}^{-1} \text{ NH}_4\text{Cl}$  and  $0.1 \text{ mol} \cdot \text{l}^{-1} \text{ NH}_3 \cdot \text{H}_2\text{O}$ , the molar ratio equal to 0.25) with different initial  $\text{Li}^+$  concentration for about 72 h at 303 K. The final adsorption isotherm is simulated according to Freundlich equation of  $Q_e = k \cdot C_e^{1/n}$ . The  $\text{Li}^+$  adsorption kinetics is carried out by stirring ( $150 \text{ r} \cdot \text{min}^{-1}$ ) about 100 mg ion-sieve in 100 ml LiCl solution (pH = 10.1) with uniform initial  $\text{Li}^+$  concentration ( $10.0 \text{ mmol} \cdot \text{l}^{-1}$ ) at 303 K. The final adsorption kinetics is simulated according to the first order rate Lagergren equation of  $\ln(Q_e - Q_t) = \ln Q_e - k_{\text{ads}} \cdot t$ . The selectivity of  $\text{Li}^+$  compared with other coexisting cations is carried out by stirring about 100 mg ion-sieve in 10 ml mixed solution (pH = 10.1) containing  $\text{Li}^+$ ,  $\text{Na}^+$ ,  $\text{K}^+$ ,  $\text{Ca}^{2+}$  and  $\text{Mg}^{2+}$  of  $10.0 \text{ mmol} \cdot \text{l}^{-1}$  respectively for 72 h at 303 K. The concentration of all metal ions in supernatant lucid solution is determined *in situ* by IC until the attainment of equilibrium. The exchange capacity or the amount of metal ion adsorbed per gram of ion-sieve at equilibrium ( $Q_e$ ), distribution coefficient ( $K_d$ ), separation factor ( $\alpha_{\text{Me}}^{\text{Li}}$ ) and concentration factor (CF) are calculated according to equations (5)-(8).

$$Q_e = (C_0 - C_e) \cdot V / W \quad (5)$$

$$K_d = (C_0 - C_e) \cdot V / (C_e \cdot W) \quad (6)$$

$$\alpha_{\text{Me}}^{\text{Li}} = K_d(\text{Li}) / K_d(\text{Me}) \quad \text{Me: Li, Na, K, Ca and Mg} \quad (7)$$

$$\text{CF} = Q_e(\text{Me}) / C_0(\text{Me}) \quad (8)$$

## 3 RESULTS AND DISCUSSION

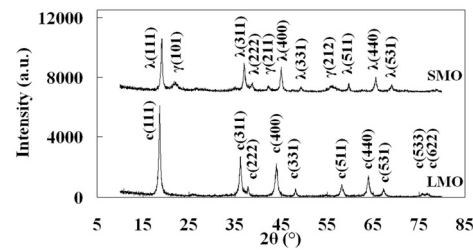


Figure 1: XRD patterns of LMO precursor and SMO ion-sieve. c(hkl): cubic  $\text{LiMn}_2\text{O}_4$  crystal face;  $\lambda$ (hkl): cubic  $\text{MnO}_2$  crystal face; r(hkl): ramsdellite  $\text{MnO}_2$ .

The powder X-ray diffraction patterns of the nanocrystal  $\text{LiMn}_2\text{O}_4$  precursor (LMO) and  $\text{MnO}_2$  ion-sieve (SMO) are presented in Figure 1. The reflections of LMO can be readily indexed to pure cubic phase [S.G.: Fd3m(227)] of  $\text{LiMn}_2\text{O}_4$  with lattice constant of  $a = 8.248 \text{ \AA}$  (JCPDS 35-0782), and the reflections of SMO, to cubic phase [S.G.: Fd3m(227)] of  $\lambda$ - $\text{MnO}_2$  with lattice constant  $a = 8.030 \text{ \AA}$  (JCPDS 44-0992). The several faint diffraction peaks at  $22.16^\circ$ ,  $42.44^\circ$  and  $56.24^\circ$  indicate trace amounts of orthorhombic phase [S.G.: Pnma(62)] of ramsdellite- $\text{MnO}_2$  (JCPDS 39-0375,  $a = 9.270 \text{ \AA}$ ,  $b = 2.866 \text{ \AA}$ ,  $c = 4.533 \text{ \AA}$ ). The phenomena are different from those of spinel  $\text{LiMn}_2\text{O}_4$  prepared by calcination method in related work, in which the  $\text{LiMn}_2\text{O}_4$  precursor and the final  $\text{MnO}_2$  ion-sieve fully present the same spinel-type structure and the relative peak intensities corresponding to (111) and (400) planes are also weaker [10]. These are probably resulted from the relatively low stability of  $\text{LiMn}_2\text{O}_4$  without high temperature crystallization process and further research to obtain pure cubic phase  $\text{MnO}_2$  ion-sieve is still in process. However, it should be noticed that the XRD patterns of LMO and SMO are still quite similar, indicating that the Mn-O lattice is stable during the  $\text{Li}^+$  extraction process and the locations of manganese in the crystal structure are well maintained as the  $\text{LiMn}_2\text{O}_4$  counterpart of solid-phase reaction.

The present synthesis conditions have been greatly alleviated and the morphology of the  $\text{LiMn}_2\text{O}_4$  precursor and final  $\text{MnO}_2$  ion-sieve is effectively controlled within low-dimensional nanorod structure as shown in Figure 2. The  $\text{LiMn}_2\text{O}_4$  precursor yields mainly mono-dispersed nanorods with about 20 nm in diameter and several micrometers in length as shown in Figure 2 LMO (A), implying that the soft chemistry synthesis is effect for the direct formation of low-dimensional  $\text{LiMn}_2\text{O}_4$  ternary nanostructure with quite uniform geometry, evidenced further by the pore size distribution curve obtained from the BJH deposition curve (as shown in Figure 3) with a pore size distribution centered on 30.9 nm. The pore size distribution, unlike the HRTEM observations, is obtained statistically, thus the appearance of the obviously broad peak is attributed to capillary condensation in the slit-

shaped meso-pores with parallel walls and implies the separation of most nanorods from one another although some of the nanorods look thicker than others. Figure 2 LMO (B) is a typical HRTEM image of a single  $\text{LiMn}_2\text{O}_4$  nanorod with inset of SAED pattern recorded on the selected area, showing reflection characteristic of one-dimensional nanorod structure, with the diffraction spots elongated in the direction perpendicular to the rod axis, and the SAED pattern also confirms that the  $\text{LiMn}_2\text{O}_4$  ternary oxide is single crystal. The SMO ion-sieve affords the similar one-dimensional nanorod morphology with  $\text{LiMn}_2\text{O}_4$  precursor as shown in Figure 2 SMO (A), without aggregation after the acid treatment process evidenced further by the pore size distribution curve (as shown in Figure 3) with a pore size distribution centered on 31.9 nm. Figure 2 SMO (B) is a typical HRTEM image of a single  $\text{MnO}_2$  nanorod with the diameter of about 20 nm and the corresponding SAED pattern (inset) indicating that the nanorod is single crystal with the growth direction along the (111) lattice face (as shown in the arrow direction).

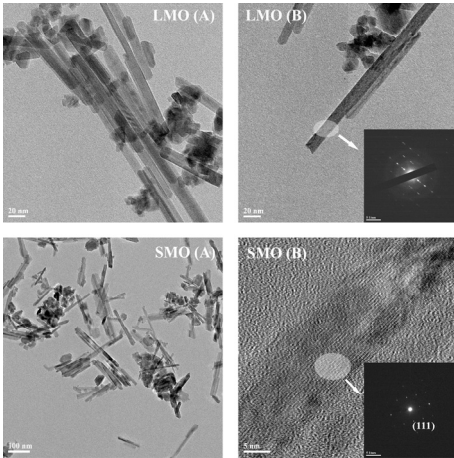


Figure 2: HRTEM images of LMO precursor and the SMO ion-sieve with the insets of SAED patterns respectively.

Figure 3 shows the  $\text{N}_2$  adsorption-desorption isotherm of LMO precursor and SMO ion-sieve. The  $\text{N}_2$  adsorption capacity of SMO ion-sieve ( $310 \text{ cm}^3 \cdot \text{g}^{-1}$ , STP) is much larger than that of LMO precursor ( $170 \text{ cm}^3 \cdot \text{g}^{-1}$ , STP), indicating that more meso-pores are developed after  $\text{Li}^+$  extracted from the precursor. In both cases, the isotherm contains H3-type hysteresis loop with a delayed desorption branch generally occurred for capillary adsorption into interstices of compact meso-pores. The physical chemistry texture property of LMO precursor and the SMO ion-sieve are shown in Table 1. The specific surface areas ( $S_{\text{BET}}$ ) accordingly increased from  $57.85 \text{ m}^2 \cdot \text{g}^{-1}$  of the  $\text{LiMn}_2\text{O}_4$  precursor to  $75.75 \text{ m}^2 \cdot \text{g}^{-1}$  of the final  $\text{MnO}_2$  ion-sieve after  $\text{Li}^+$  are extracted from the Li-Mn-O lattice, contrast to the phenomena of solid-phase reaction process, in which high temperature calcinations resulted in serious aggregation of the  $\text{LiMn}_2\text{O}_4$  and  $\text{MnO}_2$  bulky particles. Pore size distribution analysis via the DFT method, applicable for a

complete range of pore size indicates that both the samples afforded a mesoporous size distribution with the peak pore size ( $D_p$ ) centered on 30.9 nm of LMO and 31.9 nm of SMO respectively. In both cases, the values of external surface area ( $S_e$ ) and  $S_{\text{BET}}$  are similar, reflecting again the lack of micropores in these samples and the very little micropore volume is also observed.

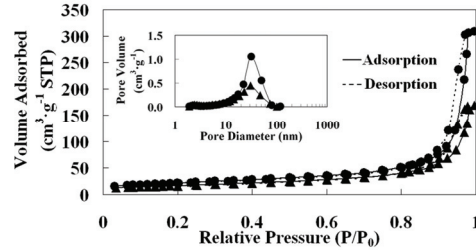


Figure 3:  $\text{N}_2$  adsorption-desorption isotherm and pore size distribution curve (inset) of LMO and SMO. ●: LMO, ▲: SMO.

	$S_{\text{BET}}$ $\text{m}^2 \cdot \text{g}^{-1}$	$S_e$ $\text{m}^2 \cdot \text{g}^{-1}$	$V_T$ $\text{cm}^3 \cdot \text{g}^{-1}$	Hysteresis Loop	$D_p$ nm
LMO	57.85	55.56	0.18	H3	30.9
SMO	75.75	72.94	0.34	H3	31.9

Table 1: Physical chemistry texture of LMO precursor and SMO ion-sieve

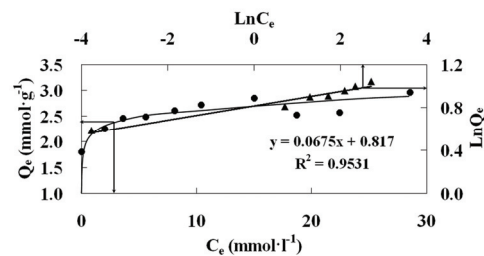


Figure 4:  $\text{Li}^+$  adsorption isotherm of SMO nanorod ion-sieve and simulation according to Freundlich equation.  $T = 303 \text{ K}$ ,  $\text{pH} = 10.1$ ,  $V = 100 \text{ ml}$ ,  $W = 100 \text{ mg}$ .

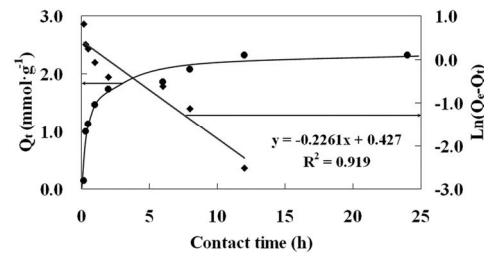


Figure 5:  $\text{Li}^+$  adsorption kinetics of SMO nanorod ion-sieve and simulation according to Lagergren equation.  $T = 303 \text{ K}$ ,  $\text{pH} = 10.1$ ,  $V = 100 \text{ ml}$ ,  $W = 100 \text{ mg}$ ,  $C_0 = 10 \text{ mmol} \cdot \text{l}^{-1}$ .

Figure 4 shows the  $\text{Li}^+$  adsorption isotherm of the SMO nanorod ion-sieve and simulation according to Freundlich equation. The data present linearity with the congruence of  $R^2 = 0.9531$ , indicating that the  $\text{Li}^+$  adsorption process in the experiment is accorded with the Freundlich adsorption isotherm. The adsorption constants are calculated to be  $K_f = 2.26$  and  $n = 14.81$ . Although the value is only a little higher than that of the bulky  $\text{MnO}_2$  ion-sieve ( $2.43 \text{ mmol}\cdot\text{g}^{-1}$ ) synthesized by high-temperature calcination method [10], it is probable that the current nanorod  $\text{MnO}_2$  contains trace amounts of ramsdellite- $\text{MnO}_2$  besides the cubic phase  $\text{MnO}_2$  (as shown in Fig. 1) and the ramsdellite- $\text{MnO}_2$  has great defect to the  $\text{Li}^+$  insertion process. Further research on the pure cubic phase nanorod  $\text{MnO}_2$  synthesis is undergoing. Figure 5 shows the  $\text{Li}^+$  adsorption kinetics of SMO nanorod ion-sieve and simulation according to Lagergren equation. The adsorption rate is fast till the contact time of 2 h, then the adsorption rate increases slowly and the process is close to the equilibrium. The value of the adsorption rate constant is calculated to be  $K_{\text{ads}} = 6.28 \times 10^{-5} \text{ s}^{-1}$ . The adsorption rate improves one order compared with bulky  $\text{MnO}_2$  ion-sieve ( $K_{\text{ads}} = 2.17 \times 10^{-6} \text{ s}^{-1}$ ) [10], indicating that the morphology and size of the ion-sieve have apparent influence on the  $\text{Li}^+$  adsorption rate.

Metal Ion	$Q_c$ $\text{mmol}\cdot\text{g}^{-1}$	$K_d$ $\text{ml}\cdot\text{g}^{-1}$	$\alpha_{\text{Me}}^{\text{Li}}$	CF $\times 10^{-3} \text{ l}\cdot\text{g}^{-1}$
$\text{Li}^+$	0.967	16770.63	1.00	95.42
$\text{Na}^+$	0.009	1.07	15640.12	1.06
$\text{K}^+$	0.004	0.46	36066.14	0.46
$\text{Mg}^{2+}$	0.126	15.47	1084.27	13.32
$\text{Ca}^{2+}$	0.230	32.26	519.80	24.15

Table 2: Adsorption selectivity of  $\text{Li}^+$  on SMO ion-sieve.

Table 2 shows the selectivity of  $\text{Li}^+$  compared with uptake behaviors of other coexisting ions in brine including  $\text{Na}^+$ ,  $\text{K}^+$ ,  $\text{Ca}^{2+}$  and  $\text{Mg}^{2+}$ . The equilibrium distribution coefficients  $K_d$  are in the order of  $\text{Li}^+ \gg \text{Ca}^{2+} > \text{Mg}^{2+} > \text{Na}^+ > \text{K}^+$ , indicating high selectivity for  $\text{Li}^+$ , but much less for  $\text{Na}^+$ ,  $\text{K}^+$ ,  $\text{Ca}^{2+}$ , and  $\text{Mg}^{2+}$ , similar to the cases of the  $\text{MnO}_2$  ion-sieves prepared by solid-phase reaction, yet there exist more obvious discriminations among the values of  $K_d$  and  $\alpha_{\text{Me}}^{\text{Li}}$ . The distribution coefficients for  $\text{Li}^+$  is  $K_{d, \text{Li}} = 16770.63 \text{ ml}\cdot\text{g}^{-1}$ , increased about 2.12 times compared with the bulky  $\text{MnO}_2$  ion-sieve ( $K_{d, \text{Li}} = 7917.49 \text{ ml}\cdot\text{g}^{-1}$ ) [10], indicating the remarkable improvement of the ion-sieve selectivity by the well-maintained nanorod structure. The results also indicate that  $\text{Na}^+$ ,  $\text{K}^+$ ,  $\text{Ca}^{2+}$  and  $\text{Mg}^{2+}$  in solution do not interfere with  $\text{Li}^+$  during the adsorption/ion-exchange process since high concentration factor (CF) values of  $\text{Li}^+$  are observed as compared with CF values of other metal ions [11].

## 4 CONCLUSION

One-dimensional spinel-type  $\text{LiMn}_2\text{O}_4$  nanorod oxide, with the average size about 20 nm in diameter and several micrometers in length, has been directly synthesized via a simple hydrothermal synthesis of commercial  $\text{Mn}(\text{NO}_3)_2$ ,  $\text{LiOH}$  and  $\text{H}_2\text{O}_2$  mixed solution at 383 K for 8 h, more favourable to control the nanocrystalline structure with well-defined pore size distribution and high surface area than traditional calcinations method, which is of great interest as an electrode material for rechargeable lithium-ion batteries. Further, the final  $\text{MnO}_2$  ion-sieve with lithium ion selective adsorption capacity could be easily prepared via the acid treatment process to completely extract lithium ions from the spinel  $\text{Li-Mn-O}$  precursor, without obvious change to the  $\text{Mn-O}$  lattice structure and the one-dimensional nanorod morphology; the  $\text{Li}^+$  selective adsorption behaviors of the  $\text{MnO}_2$  nanorod ion-sieve are improved compared with those prepared by the conventional calcinations method, which is promising in the lithium extraction from brine or seawater.

## ACKNOWLEDGMENTS

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